Chapter 2
Aspects of the Biology and Physics Underlying Modified Atmosphere Packaging

Theopanes Solomos

2.1 Introduction

The practice of modified atmosphere packaging (MAP) for fresh and minimally processed refrigerated (MPR) fruits and vegetables is widespread, particularly for commodities with a relatively short storage life (Cameron 1989; Chinnan 1989; Hayakawa et al. 1975; Hobson and Burton 1989; Kader 1986). The subject has been reviewed in the past from both a practical and a theoretical standpoint (Chinnan 1989; Mannapperuma et al. 1991). The beneficial effects of MAP are due in part to the decrease in O₂ and the increase in CO₂ levels, and in part to the decrease in water loss (Ben-Yehoshua et al. 1983; Biale 1946, 1960; Fidler et al. 1973; Isenberg 1979; Kader 1980, 1986; Kidd and West 1945; Lipton and Harris 1974; Smock 1979). In fact, in non-climacteric fruits such as citrus, the prevention of water loss is the main factor contributing to the extension of their storage life (Ben-Yehoshua et al. 1983) (see Chaps. 5, 6 and 7 for packaging materials).

In order to develop an appropriate modified atmosphere (MA) environment, the rates of O₂ uptake and CO₂ evolution, along with the permeability to O₂ and CO₂ of the film, must be known. In addition, the tolerance of the plant materials to the levels of CO₂ and O₂ engendered by MA must also be considered. The optimum levels of O₂ and CO₂ are known for a number of commodities (Fidler et al. 1973; Isenberg 1979; Kader 1985; Saltveit 1989; Smock 1979). In the case of bulky plant organs such as fruits, it is advantageous to determine the diffusivity of O₂ and CO₂ through their skin and flesh in order to avoid the creation of partial anoxia at the center of the tissue as this would be expected to contribute to spoilage and development of off-flavors during extended shelf life periods (Kader 1986).
In this chapter, we discuss aspects of both the biology and physics involved in MAP. We also attempt to address some problems encountered in the generation of non-steady-state predictive models.

2.2 Biological Responses of Plant Tissue to Low O₂ or High CO₂

2.2.1 Effects of Low O₂ on Senescence of Detached Plant Tissues

The effects of O₂ on fruit ripening include (1) a diminution in the rate of respiration, (2) a delay in the climacteric onset of the rise in ethylene, and (3) a decrease in the rate of ripening (Blackman 1954; Burg and Burg 1967; Fidler et al. 1973; Kader 1986; Kanellis et al. 1991; Mapson and Robinson 1966; Smock 1979; Solomos 1982; Yang and Chinnan 1988a, b). It was observed by Blackman (1954) that the respiratory isotherms of O₂ uptake as a function of the external O₂ concentration are biphasic in nature in that they include an initial gradual decrease at relatively high O₂ levels, followed by a rapid decline as the levels of O₂ approach zero. The isotherm of CO₂ output follows that of O₂ up to the point where the rate of decline diminishes; in fact, it may even increase as the O₂ level approaches zero (Biale 1960). The rise in CO₂ evolution at low levels of O₂ is obviously caused by the expected Pasteur effect which results in an increase in fermentation. As far as prolonging storage life is concerned, the range of O₂ levels that would be expected to be beneficial must be in the region between the point that induces the initial decline in respiration and that at which it generates partial anoxic environments. It should be underlined that in this region of O₂ levels, the tissue does not experience anoxia because (1) there is no accumulation of ethanol (Table 2.1) and (2) no symptoms of low-O₂ injury develop even after lengthy storage (Fidler et al. 1973; Kader 1986; Lougheed 1987).

Table 2.1 Ethanol content (mM)

<table>
<thead>
<tr>
<th>Apple no.</th>
<th>Air</th>
<th>Apple no.</th>
<th>1.5% O₂</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>3.294</td>
<td>1</td>
<td>1.32</td>
</tr>
<tr>
<td>2</td>
<td>3.422</td>
<td>2</td>
<td>0.56</td>
</tr>
<tr>
<td>3</td>
<td>9.264</td>
<td>3</td>
<td>0.09</td>
</tr>
<tr>
<td>4</td>
<td>5.361</td>
<td>4</td>
<td>2.18</td>
</tr>
<tr>
<td>5</td>
<td>5.584</td>
<td>5</td>
<td>0.54</td>
</tr>
<tr>
<td>Avg</td>
<td>5.385</td>
<td>Avg</td>
<td>0.938</td>
</tr>
</tbody>
</table>

“Gala” apples were kept for 180 days in air and 1.5% O₂
The biphasic nature of the O2 isotherm as a function of external O2 concentration has been attributed in turn to:

1. The existence of regulatory enzyme(s) that perceive(s) the level of O2 and exert(s) a feedback inhibition on the initial steps of glucose oxidation, thus lowering respiration (Blackman 1954; Solomos 1982; Tucker and Laties 1985)
2. The effect of resistance to the diffusion of O2 through the tissue (Chevillotte 1973; James 1953)
3. The presence of a terminal “oxidase” with an affinity for O2 much smaller than that of cytochrome oxidase (Mapson and Burton 1962)

Work with apples and avocados (Solomos 1982; Tucker and Laties 1985) has shown that suggestion (2) is not a viable explanation of the biphasic nature of the O2 isotherm. Suggestion (3), that the decrease in respiration at relatively high O2 levels is due to the presence of an oxidase other than cytochrome oxidase, is difficult to assess. It is fair to say that neither cytochrome oxidase nor the alternative oxidase is expected to be curtailed by the levels of O2 that initiate a diminution in the rate of respiration. Table 2.2 presents data that indicate that the apparent \( K_m \) for O2 of the putative oxidase must be larger than 4 \( \mu \)M in order to produce an experimentally detectable decrease in CO2 evolution. It is known that the \( K_m \) for O2 of the cytochrome oxidase is about 0.05 \( \mu \)M, whereas that of the alternative oxidase is 10- to 15-fold higher than that of cytochrome oxidase (Douce 1985; Siedow 1982; Solomos 1977; Tucker and Laties 1985). The data thus preclude the curtailment of either of the known mitochondrial terminal oxidases by relatively high O2 concentrations. Plant tissues, however, contain terminal “oxidases” that are resistant to the combined inhibition of both cytochrome and alternative oxidase (Laties 1982; Theologis and Laties 1978). Neither the nature of the residual oxidases nor the degree of their participation in plant respiration is known with any degree of precision. Suffice it to say that they are predominantly cytosolic in origin, with rather a low affinity for O2 (Solomos 1988). Because of this low O2 affinity, it could be argued that these

### Table 2.2 Internal O2 concentration, rate of respiration, and percentage of \( V_{\text{max}} \) of oxidases with different \( K_m^{O_2} \)

<table>
<thead>
<tr>
<th>Intercellular partial pressure of O2 kPa</th>
<th>CO2 output (( \mu )l·g(^{-1})·h(^{-1}))</th>
<th>( K_m^{O_2} ) (( \mu )M)</th>
<th>Percentage of ( V_{\text{max}} )</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td></td>
<td>0.05</td>
<td>2.2</td>
</tr>
<tr>
<td>19.25</td>
<td>5.92</td>
<td>99.98</td>
<td>99.45</td>
</tr>
<tr>
<td>6.50</td>
<td>5.90</td>
<td>99.94</td>
<td>99.13</td>
</tr>
<tr>
<td>4.91</td>
<td>4.92</td>
<td>99.91</td>
<td>97.47</td>
</tr>
<tr>
<td>4.13</td>
<td>4.40</td>
<td>99.90</td>
<td>96.96</td>
</tr>
<tr>
<td>2.23</td>
<td>3.34</td>
<td>99.78</td>
<td>93.81</td>
</tr>
<tr>
<td>0.92</td>
<td>3.30</td>
<td>98.82</td>
<td>73.60</td>
</tr>
<tr>
<td>0.49</td>
<td>2.20</td>
<td>85.63</td>
<td>16.57</td>
</tr>
</tbody>
</table>

The data were calculated from the rate of respiration and diffusion coefficient of O2 through the skin and flesh of “Gold” apples (Solomos 1987)
“oxidases” may not be contributing to the decrease in respiration with decreasing external O$_2$ levels. It should be emphasized that in actively respiring plant tissues, such as avocados, the O$_2$ level is low enough to preclude any appreciable participation of the residual oxidases in the respiration of the fruit. Even in potato tubers, which have much lower rates of respiration than avocado fruits (Solomos and Laties 1976), the oxygen level at the center of the tuber drops to about 13% (Fig. 2.1), a concentration that would be expected to severely curtail the engagement of these “residual” oxidases (Solomos 1988). In addition, their curtailment must exert a feedback restraint on the initial steps of glucose oxidation, yet this is not compatible with the most likely known regulatory mechanisms of plant respiration (Davies 1980; Solomos 1988; Turner and Turner 1980; Wiskich 1980). In the case of climacteric fruits, it may be suggested that the effect of low O$_2$ on respiration is due to the diminution of ethylene action (Burg and Burg 1967). Therefore, on the basis of the above discussion, it appears that suggestion (1) is the most likely explanation of the effects of low O$_2$ on fruit respiration.

It was assumed in the past that the accompanying decrease in respiration in response to a lowering of the external O$_2$ levels was an important facet of the mode of action of low O$_2$ in prolonging the storage life of fruits (Burton 1974). However, one may argue that the decrease in respiration reflects a metabolic depression engendered by hypoxia. In the first place, hypoxia affects metabolic events in tissues where ripening is not an issue and where ethylene is not involved. For instance, hypoxic conditions inhibited the accumulation of RNA, protein, and DNA synthesis associated with the wounding of potato tubers (Butler et al. 1990). We have also

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**Fig. 2.1** Oxygen distribution along the tuber. The oxygen distribution was calculated from the data concerning the diffusivity of CO$_2$ in the skin and flesh of potato tubers (Tables 2.11 and 2.12) and the assumption that the sum of the internal partial pressures of CO$_2$ and O$_2$ equals the partial pressure of the latter in the ambient atmosphere.
observed that hypoxia (1.5% O₂) prevented the accumulation of simple sugars and the induction of the alternative oxidase associated with storage of potato tubers at 1 °C (Table 2.3). It should be pointed out that in potatoes, chilling temperatures do not induce the biosynthesis of ethylene. Undoubtedly the delaying effects of low O₂ on the senescence of detached plant organs in general, and fruit ripening in particular, must involve a decrease in ethylene accumulation. In a perceptive paper, Burg and Burg (1967) suggested that the ethylene receptor contains a metal and when it is in its oxidized state, the binding of ethylene is enhanced. However, the effect of hypoxia on ethylene biosynthesis and action may be indirect through the suppressive effects of hypoxia on the induction of 1-amino-cyclopropane-1-carboxylic acid (ACC) synthase and/or synthesis of transducer(s) of ethylene action. It has been reported previously that, in avocados, O₂ concentrations in the range of 2.5–5.5% suppress the activity, appearance of exoenzymes, and accumulation of proteins of cellulose and polygalacturonase, associated with normal ripening (Kanellis et al. 1991). The suppressive effects on the cellulase protein were also reflected in the accumulation of its mRNA. Further, the intensity of inhibition of the synthesis of these hydrolases was inversely related to the levels of O₂ under which the fruits were kept. In addition, the same range of O₂ concentrations that suppressed the synthesis of the hydrolases induced the appearance of anaerobic isoenzymes of alcohol dehydrogenase (ADH). The rates of increase in the levels of cellulose, its mRNA and polygalacturonase, and the disappearance of the anoxic isoenzymes of ADH on reexposure of the fruits to air were directly related to the previous levels of O₂ (Kanellis et al. 1991). The fact that similar ranges of O₂ concentrations on one hand suppressed the rise in the enzymes associated with normal ripening, while at the same time inducing the synthesis of anoxic isoenzymes of ADH, indicates that the O₂ sensing mechanism is common for both processes. The induction of anoxic isoenzymes in response to hypoxia is easily understood because it is advantageous for the tissue to synthesize enzymes that increase the production of ATP in anoxia before oxygen is completely depleted. However, the extension of the storage life of fresh fruits and vegetables must be the consequence of metabolic depression which, unlike anoxia, is not deleterious to the long-term survival of the tissue. Metabolic depression is the most important adaptation for survival of intertidal organisms, which experience frequent transitions from normoxia to hypoxia (Storey and Storey 1990). Because the intensity of respiration could be considered to reflect the intensity

<table>
<thead>
<tr>
<th>Days</th>
<th>Sugars (μmoles·g⁻¹)</th>
<th>Alternative oxidase nanomoles O₂·min⁻¹·mg protein⁻¹</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>10 °C Air</td>
<td>1 °C Air</td>
</tr>
<tr>
<td>0</td>
<td>16.9</td>
<td>–</td>
</tr>
<tr>
<td>20</td>
<td>19.6</td>
<td>91.5</td>
</tr>
<tr>
<td>30</td>
<td>18.4</td>
<td>113.4</td>
</tr>
</tbody>
</table>

Table 2.3 Effect of 1.5% O₂ on sugar accumulation and activity of the alternative oxidase in potato tubers stored at 1°C
of cellular metabolism, and because low oxygen invariably decreases the rate of respiration of such detached plant organs as fruits, flowers, and leaves, this indicates that hypoxia, by an as yet unknown mechanism, produces a decrease in metabolism, which in turn results in diminishing the rate of plant development and hence senescence. In short, the decrease in respiration may not be the cause of the decline in the rate of senescence, but rather a response to a metabolic depression, which diminishes the demand for biological energy.

It has been pointed out that low O$_2$ in preclimacteric tissues delays the onset of the climacteric rise in ethylene evolution (Mapson and Robinson 1966). Experimental results concerning the range of O$_2$ concentrations that delay the onset of ripening are limited. It appears that in the case of “Gala” apples, the external O$_2$ concentration must fall below 8% in order to prolong the preclimacteric stage of the apples (Table 2.4). In short, the system that is involved in the induction of ACC synthase, a key regulatory enzyme in ethylene biosynthesis (Yang and Hoffman 1984), is saturated at O$_2$ levels above 7–8%. The data of Table 2.4 show, as expected, that the effect of low O$_2$ on the timing of the onset of ripening differs with the season.

Quantitative data concerning the effect of low O$_2$ on the rate of ripening are rather difficult to establish. At present it is not possible to describe unequivocally the relationships between O$_2$ concentration and rate of ripening. Suffice it to say that low O$_2$ does indeed delay ripening, as has been amply demonstrated in a variety of fruits (Kader 1986; Knee 1980; Kanellis et al. 1991; Liu and Long-Jum 1986; Quazi and Freebairn 1970; Yang and Chinnan 1988a). Yang and Chinnan (1988b) developed a mathematical expression for predicting the changes in the color of tomato fruits as a function of O$_2$ concentration.

A critical parameter that must be taken into consideration in designing suitable MAP is the limit of O$_2$ below which the produce cannot be safely stored. This limit, as expected, varies with the produce, but it is important to realize that levels of O$_2$ that induce partial anaerobiosis will be detrimental to both longevity and quality of the produce. This limit can be assessed experimentally by measuring either the values of the respiratory quotient (RQ) or, preferably, the increase in ethanol content of the tissue. The latter may be a more reliable indicator than the RQ values, especially at levels of O$_2$ that initiate partial anaerobiosis, and that will be somewhat difficult to detect from the changes in the RQ. Because of its volatility, ethanol can be detected in the ambient atmosphere of MAP by removing a gas sample and determining the ethanol content using gas chromatography (Nakhasi et al. 1991).

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**Table 2.4** Days to climacteric under different O$_2$ concentrations

<table>
<thead>
<tr>
<th>Year</th>
<th>Harvest date</th>
<th>Treatment</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>Air 8% O$_2$</td>
<td>6% O$_2$</td>
</tr>
<tr>
<td>1987</td>
<td>8–24</td>
<td>19 24</td>
</tr>
<tr>
<td>1988</td>
<td>8–26</td>
<td>22 –</td>
</tr>
<tr>
<td>1989</td>
<td>8–22</td>
<td>21 –</td>
</tr>
<tr>
<td>1990</td>
<td>8–24</td>
<td>16 –</td>
</tr>
<tr>
<td>1991</td>
<td>8–27</td>
<td>9 –</td>
</tr>
</tbody>
</table>
2.2.2 Effects of CO₂ on Senescence of Detached Plant Tissues

The mode of action of CO₂ on senescence is unclear. Burg and Burg (1967) suggested that CO₂ is a competitive inhibitor of ethylene. Recent experimental evidence indicates that CO₂ may indeed diminish the action of ethylene provided the concentration of the latter is less than 1 μL·L⁻¹. In the case of apples, CO₂ enhances the inhibitory effects of low O₂ on respiration (Fidler et al. 1973), whereas CO₂ concentrations in the range of 1–27% do not affect the rate of respiration of peaches (Deily and Rizvi 1982). It should be pointed out that CO₂ is a metabolically active molecule participating in a number of carboxylating reactions. In addition, it is expected that high concentrations of CO₂ could alter the pH of the cytosol, which in turn may affect plant metabolism (Siripanich and Kader 1986). Anoxic conditions generated by CO₂ induce changes in a number of intermediate metabolites that differ from those observed when the tissue is kept under nitrogen instead (Kader, personal communication). CO₂ is also required for the action of ACC oxidase (Kuai and Dilley 1992).

It is well known that tolerance to CO₂ varies greatly, not only between species but also between cultivars of the same species. For instance, “Golden Delicious” apples can tolerate high CO₂ concentrations, whereas “McIntosh” apples are damaged by even 3% CO₂ (Fidler et al. 1973). Strawberries can tolerate CO₂ levels as high as 20%, and storage of peaches in 10–15% CO₂ is beneficial (Deily and Rizvi 1982). In apples, high CO₂ concentrations appear to inhibit succinic acid dehydrogenase (Hulme 1956). Storage of lemons under high concentrations of CO₂ leads to an accumulation of organic acids (Biale 1960). In lettuce, high CO₂ concentrations affect the metabolism of phenolic compounds (Siripanich and Kader 1985a, b). Another beneficial effect of high CO₂ levels is their antimicrobial activity. At present it is impossible to predict the tolerance of a particular tissue to high levels of CO₂ (Kader 1986).

2.2.3 Effects of Slicing on Tissue Metabolism

The effects of wounding on plant metabolism have been studied extensively in tissues prepared from bulky plant organs such as tubers and roots. The vast literature on this subject has established that slicing induces profound quantitative and qualitative changes in tissue metabolism (Kahl 1974; Laties 1978). The observed changes include a rise in respiration, DNA and RNA synthesis, induction of new enzymes, membrane degradation, and the appearance of novel mRNA (apRees and Beevers 1960; Butler et al. 1990; Clicke and Hackett 1963; Kahl 1974; Laties 1978). The effect of slicing on respiration is probably the most extensively studied aspect of wounding in bulky plant organs (Laties 1978). These investigations have shown that slicing induces a three- to fivefold rise in respiration over that of the parent-plant organ. With aging there is a further two- to threefold increase in respiration (Laties 1978). This rise in respiration with aging of slices is critically dependent on
protein and RNA synthesis since the addition, within 8–10 h of slicing, of either protein or RNA synthesis inhibitors prevents the development of the respiratory rise with aging (Clicke and Hackett 1963; Kahl 1974). Neither the cause of this rise in respiration nor its metabolic significance is clear. However, the data indicate that inhibitors of respiratory development also inhibit a number of biochemical events, such as suberin formation and synthesis of phenolics, associated with aging of potato slices (Kahl 1974; Laties 1978).

Several experiments show that the nature of both respiratory substrates and pathways changes with aging of slices. In particular, in fresh potato slices, most of the respiratory CO$_2$ is derived from the $\alpha$-oxidation of fatty acids arising out of the attendant breakdown of phospholipids in response to slicing, whereas carbohydrates are respiratory substrates of aged slices (Jacobson et al. 1970; Laties 1978). It has also been reported that in slices other than potatoes, a large portion of CO$_2$ is produced by the pentose phosphate pathway (PPP) (apRees and Beevers 1960). In addition it should be mentioned that temperature and gas composition affect both respiratory substrates and pathways. Thus, when potato slices are aged either in air, in the presence of 10% CO$_2$, or in a bicarbonate solution, suberin formation is prevented and the tissue develops callus (cf. Laties 1978). Moreover, the respiration of aged slices is manolate resistant and is presumed to comprise the PPP (Kahl 1974). This observation is important from the point of view of MAP because aging in high CO$_2$ levels may prevent the formation of color in potato slices.

The effects of hypoxia on minimally processed produce, in combination with high CO$_2$ concentrations, have not been studied in detail. However, based on the observations that hypoxia inhibits the synthesis of DNA, protein, and novel mRNA in potato slices (Butler et al. 1990), it may be anticipated that these conditions repress the synthesis of those enzymes that are considered to exert adverse effects on the quality of tissue slices, for example, phenylalanine ammonia lyase (PAL), this being considered to increase the content of phenolics in the tissue, which in turn tend to increase in wounded plant tissues (Kahl 1974; Uritani and Asahi 1980). In addition MAP environments may suppress the rise in amylases, thus diminishing the breakdown of starch prevalent in potato slices (Kahl 1974).

A number of experimental observations indicate that regardless of the origin of the respiratory reducing equivalents, the terminal electron acceptor is predominantly cytochrome oxidase, even in tissues that possess substantial cyanide-resistant respiration (Laties 1978; Solomos 1988). If this is the case in tissue slices, the oxygen concentration can be reduced to very low levels because of the high affinity for O$_2$ of the cytochrome oxidase, and because of the short diffusion path available to gases. For instance, in the case of sweet potato slices suspended in air at 25 °C, the rate of O$_2$ uptake is of zero order with respect to its external concentration until the latter drops to about 0.4% (Fig. 2.2). The ability to decrease the O$_2$ concentration to such low levels may be beneficial because it is expected to reduce the browning due to polyphenol oxidases (PPO), as the latter have a rather high $K_m$ for O$_2$ (Beevers 1961).

At present there are no detailed studies concerning the effect of ranges of O$_2$ and/or CO$_2$ concentrations on either metabolism, longevity, or quality of cut tissue segments. It is to be expected, as in the case of intact tissues, that O$_2$ concentrations
that engender partial anoxia will be detrimental to longevity and quality of the produce. This low limit of O₂ can be assessed in a manner identical to that described earlier for intact tissues.

### 2.3 Determination of Gas Diffusivities in Plant Tissues

#### 2.3.1 General Considerations

In attempting to generate predictive MAP models, it is useful to know the tissue’s permeability to gases in order to calculate their concentration at the center of the organ, particularly when bulky fruits or vegetables are used. The diffusion barriers of a plant organ include the skin, the intercellular spaces, the cell walls, and plasma-lemma. The diffusion of gases through bulky plant organs such as fruits, roots, and tubers follows Fick’s first law, and the diffusion channels are predominantly gaseous in nature (Burg and Burg 1965; Burton 1974; Cameron and Yang 1980; Solomos 1987). Simple calculations with apples have shown that, assuming an aqueous diffusion barrier, the maximum radius that could maintain 1% O₂ at the center of the fruit would be about 0.7 cm (Solomos 1987). For fruits with rates of O₂ uptake much larger than that of apples, the radius would be even smaller. Similar observations have also been reported for potato tubers and apples (Burton 1974).

![Diagram](image)

**Fig. 2.2** The rate of O₂ uptake of slices suspended in air was followed polarographically. The slices were initially maintained under 0.925% O₂. At the indicated point, the gas was turned off. The rate of O₂ uptake between 20.946% and 0.925% was of zero order.
The most convincing evidence for the gaseous nature of the diffusion paths is that provided by Burg and Burg (1965). These authors showed that the diffusivity of gases was inversely related to the external pressure (Table 2.5), as would be expected from the ideal gas law. If the barrier was liquid in nature, the changes in external pressure would not be expected to affect the length of the mean free path because of the incompressibility of water.

Fick’s first law states that the flux normal to the surface of a metabolically inert gas is given by (Crank 1970):

$$J = AD \frac{\partial c}{\partial x}$$  \hspace{1cm} (2.1)

where $J$, in μmoles sec$^{-1}$ per fruit, is the flux; $A$, in cm$^2$, is the surface available to diffusion; $D$, in cm$^2$ sec$^{-1}$, is the diffusion coefficient; and $\partial c/\partial x$ is the concentration gradient with respect to distance. It is customary to replace $\partial c/\partial x$ with the difference in concentration $\Delta c/\Delta x$. This is permissible only when the change in concentration with distance is linear (Jacobs 1967; Nobel 1983). In order to determine $D$, the concentration gradient must first be determined. In the case of non-steady-state conditions, the change in concentration with respect to time should also be known. In order to calculate these gradients, it is necessary to solve the equation for Fick’s second law (Crank 1970; Jacobs 1967). The general equation for Fick’s second law for a metabolically active gas in three dimensions is (Crank 1970):

$$\frac{\partial c}{\partial t} = D \left[ \frac{\partial^2 c}{\partial x^2} + \frac{\partial^2 c}{\partial y^2} + \frac{\partial^2 c}{\partial z^2} \right] \pm \nu$$  \hspace{1cm} (2.2)

where $\nu$ is the specific rate of evolution (+) or uptake (−) of the gas under consideration. The analytical solutions of Eq. (2.2) are numerous, depending on the boundary conditions and the initial distribution of the gas throughout the barrier. Equations (2.3) and (2.4) below represent the expression of Eq. (2.2) for a solid sphere and cylinder, respectively (Crank 1970; Jacobs 1967):

$$\frac{\partial c}{\partial t} = D \left[ \frac{\partial^2 c}{\partial r^2} + \frac{2 \partial c}{r \partial r} \right] \pm \nu$$  \hspace{1cm} (2.3)

$$\frac{\partial c}{\partial r} = D \left[ \frac{\partial^2 c}{\partial r^2} + \frac{1 \partial c}{r \partial r} \right] \pm \nu$$  \hspace{1cm} (2.4)

<table>
<thead>
<tr>
<th>External pressure (kPa)</th>
<th>Internal ethylene concentration (μl)</th>
</tr>
</thead>
<tbody>
<tr>
<td>101.3</td>
<td>472</td>
</tr>
<tr>
<td>76</td>
<td>319</td>
</tr>
<tr>
<td>37.3</td>
<td>190</td>
</tr>
<tr>
<td>25.3</td>
<td>88</td>
</tr>
</tbody>
</table>

From Burg and Burg (1965)
where \( r \), in cm, is the radius of the sphere and cylinder. In cases where the peel of the tissue is the main parameter, these equations must be solved for hollow spherical and cylindrical shells. For nonmetabolic gases, there are analytical solutions for a hollow sphere and cylinder (Crank 1970).

Apart from the mathematical complexities, determining the diffusivity of gases under dynamical conditions introduces a number of uncertainties because of the nonhomogeneous nature of the diffusion barriers of a plant organ. For instance, the diffusion coefficients of CO\(_2\) in the skin and flesh of potato tubers are about \( 6.90 \times 10^{-7} \) and \( 2.50 \times 10^{-4} \) cm\(^2\)·sec\(^{-1}\), respectively. The existence of such a barrier in the flesh will generate appreciable concentration gradients within the flesh when the efflux of a gas is measured. To demonstrate this point, it is assumed that CO\(_2\) is diffusing in an infinite cylinder of unit cross-sectional area, with a \( D_{CO_2} \) similar to that of potato tuber flesh. Table 2.6 describes the percentage distribution of a quantity \( M \) of CO\(_2\) deposited at \( x = 0 \) and \( t = 0 \). The change in concentration with time and distance is given by (Crank 1970):

\[
C(x,t) = \frac{M}{2\pi (Dt)^{1/2}} \times \exp \left[ -\frac{x^2}{4Dt} \right]
\]

(2.5)

It may be seen from Table 2.6 that the concentration gradient is substantial. Therefore, the assumption that the concentration of a metabolically inert gas is uniform throughout the flesh is not valid (Cameron and Yang 1980).

Another uncertainty of the efflux method is the assumption that the equilibrium between the cellular solution and intercellular spaces is instantaneous. However, a number of observations indicate that this may not be the case. It was shown by Burton (1950) that the evacuation of O\(_2\) from a small plug of potato tissue was a lengthy process. In addition, indirect experimental evidence indicates that the resistance to gas diffusion from the cell to the intercellular spaces may not be negligible (Chevillotte 1973). It is also expected that the solubility of the gas in aqueous solutions would affect the equilibrium distribution between the cell and the intercellular spaces, especially where short time intervals are concerned. A case in point is the changes in RQ in the course of the rapid climacteric rise in respiration. In precli-

<table>
<thead>
<tr>
<th>Time (min)</th>
<th>Distance (cm)</th>
<th>1.5</th>
<th>2</th>
<th>2.5</th>
<th>3</th>
</tr>
</thead>
<tbody>
<tr>
<td>10</td>
<td>12.688</td>
<td>1.870</td>
<td>0.061</td>
<td>0.001</td>
<td>0.000</td>
</tr>
<tr>
<td>11</td>
<td>14.223</td>
<td>1.880</td>
<td>0.111</td>
<td>0.003</td>
<td>0.000</td>
</tr>
<tr>
<td>15</td>
<td>18.755</td>
<td>4.253</td>
<td>0.533</td>
<td>0.037</td>
<td>0.001</td>
</tr>
<tr>
<td>20</td>
<td>21.854</td>
<td>7.182</td>
<td>1.512</td>
<td>0.204</td>
<td>0.018</td>
</tr>
<tr>
<td>30</td>
<td>24.009</td>
<td>11.433</td>
<td>4.046</td>
<td>1.064</td>
<td>0.208</td>
</tr>
<tr>
<td>40</td>
<td>24.119</td>
<td>13.826</td>
<td>6.344</td>
<td>2.330</td>
<td>0.685</td>
</tr>
<tr>
<td>50</td>
<td>23.581</td>
<td>15.109</td>
<td>8.102</td>
<td>3.636</td>
<td>1.365</td>
</tr>
<tr>
<td>60</td>
<td>22.843</td>
<td>15.763</td>
<td>9.378</td>
<td>4.809</td>
<td>2.126</td>
</tr>
</tbody>
</table>
macteric avocados, the RQ is close to unity, changes to less than one at the climacteric peak, and then returns toward unity at the postclimacteric stage (Solomos and Laties 1976). It was found, however, that in bananas this pattern of changes was not metabolic in nature, but rather the result of the difference in the respective solubilities of CO₂ and O₂ in water (McMurchie et al. 1972). Because of this difference in solubilities, O₂, which has a smaller solubility in water than does CO₂, equilibrates with the intercellular spaces faster than does CO₂. Further, the efflux method requires a precise knowledge of the volume of the intercellular spaces and the solubility of the gas in the cellular liquid.

However, if appropriate experimental precautions are taken, it may be feasible to obtain reasonable approximations of gas diffusivities through the skin of a plant organ by following the efflux of metabolically inert gases. For instance, if the skin is thin, if the tissue is loaded with relatively high concentrations of the inert gas, if the volume of the vessel is small, and if the diffusion in the flesh is much larger than in the skin, then this method could give reasonable approximations of gas diffusivity through the skin. In order to avoid the generation of the concentration gradient along the flesh of potato tubers, the resistance to diffusion was calculated by considering only the initial linear part of the efflux isotherm of ethane (Banks 1985). This approach, however, introduces some uncertainties concerning the origin of the gas. It was assumed that the gas originated under the skin, which may not be correct because ethane, being nonpolar, is expected to dissolve in the waxy layers of the cuticle. In tissues with thick skin, the volume of the waxy layer can be appreciable. For instance, in a cylindrical tuber of radius 2.8 cm, length 12 cm, and skin thickness 0.012 cm, the volume of the phellem is about 2.5 ml. It is also possible that some of the initial gas efflux may originate from the gas adsorbed on the tuber surface or present in gaseous cavities. This approach could be compared to the ion fluxes, where the initial flux contains a large component of the apparent free space and does not measure fluxes across the cellular membranes, these being the main barrier to ion fluxes between cells and ambient environment (Briggs et al. 1961). It should be emphasized that any determination of gas diffusion is meaningless unless it is verified experimentally.

In view of the uncertainties and mathematical complexities involved in the determination of the $D$ of gases under non-steady-state conditions, we shall here consider only steady-state situations.

The steady-state solution of Eq. (2.2), $((\partial c)/\partial t = 0)$, in a one dimensional, plane sheet, for a metabolically active gas is (Hill 1928):

$$
C(x) = \frac{v}{2D} x^2 - \frac{\ell v}{D} x + C_0
$$

(2.6)

where $v$, in $\mu$moles cm$^{-3} \cdot$sec$^{-1}$, is the constant rate of output (+) or uptake (−) of the gas per unit tissue volume; $\ell$, in cm, is half of the tissue thickness; and $C_0$, in $\mu$moles cm$^{-3}$, is the concentration of the gas at $x = 0$, that is, the ambient atmosphere. Thus, the concentrations of CO₂ and O₂ at the center of the tissue $C_i$ are:

$$
C_i = C_0 \pm \frac{v}{2D} \ell^2
$$

(2.7)
The concentrations of CO₂ and O₂ at the center of a sphere and cylinder are given by Eqs. (2.8) and (2.9), respectively (Hill 1928):

\[ C_i = C_0 \pm \frac{V}{6D} R^2 \]  
(2.8)

\[ C_i = C_0 \pm \frac{V}{4D} R^2 \]  
(2.9)

where \( R \), in cm, is the radius of either the sphere or cylinder. The other notations have been defined earlier.

In the case of metabolically inert hollow spherical and cylindrical shells, the flux of CO₂ per unit time at their surfaces is given by Eqs. (2.10) and (2.11), respectively (Crank 1970):

\[ J = 4\pi D \frac{C_i - C_0}{R - R_i} \]  
(2.10)

\[ J = 2\pi D h \frac{C_i - C_0}{\ln \left( \frac{R}{R_i} \right)} \]  
(2.11)

where \( R \) and \( R_i \), in cm, are the outside and inside radii, respectively. In the case of a thin spherical wall (Eq. 2.10), it is assumed that \( R-R_i \approx R_2 \). The other notations have been defined earlier. It should be pointed out that Eq. (2.11) may not be very accurate unless the surfaces of the cylindrical bases are small in comparison with the cylindrical surface, and the length is much larger than the radius. In the case of oxygen, the order of the concentration differences in Eqs. (2.10) and (2.11) is reversed, for example, \( C_0 - C_i \). It is obvious from Eq. (2.11) that for an accurate determination of \( D \), the values of \( R \) and \( R_i \) must be known with some degree of precision. It is customary to use Eq. (2.12), instead of Eq. (2.11):

\[ J = 2\pi h \frac{C_i - C_0}{\Delta r} D \]  
(2.12)

and to determine the apparent diffusion coefficient, \( D' = (D/\Delta r) \). This could, depending on the dimensions, introduce appreciable error because \( D' = R \times (D/\Delta r) \) (Abdul-Baki and Solomos 1994).

Finally the flux of oxygen through a metabolically inert plane sheet is given by Eq. (2.13) (Jacobs 1967):

\[ J = \frac{AD(C_0 - C_i)}{\Delta x} \]  
(2.13)

As already mentioned, gases diffuse in and out of plant organs in gaseous channels. Thus, the usually observed low diffusivities are due to the fact that only a small
fraction of the tissue surface is available to gas diffusion. In “Russet Burbank” potato tubers, the fraction of the surface permeable to gases varies with the tuber from $4.22 \times 10^{-6}$ to $7.8 \times 10^{-6}$, the average being $6.22 \times 10^{-6}$ (Abdul-Baki and Solomos 1994). It is thus apparent that Eq. (2.1) should be written as:

$$J = ADN \frac{dc}{dx}$$

where $N$ is a number between 0 and unity representing the fraction of the surface that is permeable to gases (Burg and Burg 1965). On the basis of microscopic and gas diffusion measurements, it was calculated that only 1/1000 of the cross section of the flesh of potato tubers is permeable to gases (Woolley 1962).

The diffusivity of gases through plant tissues could also be decreased by the degree of tortuosity of the path. However, in most plant tissues of interest for consumption, the skin is quite thin; hence, the effect of a tortuous path will probably be insignificant.

It was mentioned earlier that for the determination of the diffusion coefficient of the gases for the cases considered above, one must measure the flux and the concentrations of the gases inside and outside the tissue.

### 2.3.2 Measurements of Intercellular Gases

Several methods have been used in the past to ascertain the internal concentration of gases in various fruits and vegetables. These methods include evacuation, manometric techniques, use of oxygen microelectrodes, and the removal of plugs of tissue which are then sealed in airtight vials (Solomos 1987).

The evacuation technique introduces the following uncertainties. In the first place, the values reflect the overall concentration of the gases in the tissue and not that at a particular point, for example, at the center, under the skin, etc. Further, the evacuated gases will contain not only those present in the intercellular spaces, which is required, but an unknown portion of the dissolved gases in the cellular sap. This in turn requires corrections that must include solubility of gases in the cell liquid and also, depending on time and intensity of respiration, the production or utilization of the gas within the time interval. The use of O$_2$ microelectrodes has produced measurements of some large O$_2$ gradients within the tissue (Brädle 1968). Readings of an oxygen microelectrode will vary greatly depending on whether the electrode is submerged in liquid or is in a gaseous phase. The use of manometric techniques, though reliable, requires the construction of special apparatus which makes it difficult to use for a large number of samples (Hulme 1951). Removal of plugs is a destructive method. In addition, it introduces uncertainties in the subsequent analysis of the gases similar to those given above for the evacuation technique.

Banks and Kays (1988) affixed small vials on the surface of potato lenticels and followed the changes in the concentration of CO$_2$ and O$_2$. It is expected that these concentrations in the vials will reflect that under the skin. This method is an
improvement on any of the previous techniques, but the uncertainty exists that the gases may diffuse laterally to adjacent lenticels if the pressure in the vial increases, or the lenticel is partially blocked. Waldraw and Leonard (1939) removed small plugs of tissue to create cavities into which the inserted tubes were in turn sealed airtight. It is anticipated that, with time, the composition of the gas atmospheres of the tubes will equilibrate with the internal gas atmosphere of the tissue. Thus, the composition of the fruit gases can be determined by analyzing the gas in the tubes. Trout et al. (1942) showed that the removal of up to 10 ml of gas from the internal cavity of apple fruit generated no appreciable drop in pressure, and the system returned to equilibrium quite rapidly. However, this may not be the case for plant organs with small intercellular spaces. With improved analytical techniques for measuring gases, a small volume of samples – between 25 and 50 μl – can be used to accurately determine the concentrations of metabolically active gases, that is, O₂, CO₂, and C₂H₄. Several investigators have inserted hypodermic needles into the locule cavities of apple fruits to determine the internal concentration of C₂H₄ (Burg and Burg 1965). The hubs of the needles are sealed with a vaccine cap, and samples are withdrawn from the needle using an airtight syringe. The concentration of C₂H₄ is then measured by gas chromatography (Burg and Burg 1965).

This method can be improved upon further by gluing a chromatographic septum to the calyx of the fruit and inserting the needle through the septum and into the locules (Solomos 1989). This technique facilitates sequential sampling, and the needle can be replaced easily if it becomes blocked. The method has the additional advantage that it inflicts minimal injury, and the needle can be kept in the fruit for longer periods so that the effect of injury is dissipated. In the case of fruits, such as apples, with large locular cavities, the injury effect may not be an issue. Further, because of the small volume of the needle, it is expected that its gas space will come into rapid equilibrium with the intercellular gases, and, in addition, the removal of small volumes of sample gas is expected to represent that in the intercellular spaces adjacent to the needle tip. In this way, gradients across the tissue can be ascertained.

Previous work established, as expected, that the total internal gas pressure equals that of the ambient environment (Hulme 1951; Trout et al. 1942). That requires that the sum of the internal partial pressures of the gases equals the surrounding atmosphere, approximately 1 atm. This is indeed the case for apple fruit (Table 2.7). This in turn suggests that the sampling method does not introduce appreciable experimental error. The rate of gas exchange can be measured either by a static or a flow-through system (Henig and Gilbert 1975; Solomos 1987).

<table>
<thead>
<tr>
<th>Experiment</th>
<th>CO₂</th>
<th>O₂</th>
<th>N₂</th>
<th>Total CO₂ + O₂ + N₂ + argon + water vapors</th>
</tr>
</thead>
<tbody>
<tr>
<td>Experiment 1</td>
<td>0.022</td>
<td>0.181</td>
<td>0.772</td>
<td>1.002*</td>
</tr>
<tr>
<td>Experiment 2</td>
<td>0.026</td>
<td>0.183</td>
<td>0.777</td>
<td>1.012</td>
</tr>
<tr>
<td>Experiment 3</td>
<td>0.022</td>
<td>0.188</td>
<td>0.777</td>
<td>1.014</td>
</tr>
</tbody>
</table>

*Each reading represents the average of five apples.
2.3.3 Experimental Determination of CO\textsubscript{2} Diffusivity in Apples and Potatoes

As mentioned above, the diffusion barriers from the cell to the ambient atmosphere include the skin, intercellular spaces, cell walls, and plasmalemma. Most of the previous data were mainly concerned, apart from a couple of exceptions (Burton 1950; Solomos 1987; Woolley 1962), with measuring skin resistance (Banks 1985; Burg and Burg 1965; Cameron and Yang 1980). The main reason for this is that the experimental procedures that were used are not amenable to determining gas diffusion through the intercellular spaces of the flesh. Further, with a few exceptions, the calculated resistances have not been subjected to experimental verification. We shall here briefly describe methods for evaluating gas diffusion coefficients through both skin and flesh, as well as experimental procedures for ascertaining their validity. Here we shall confine the discussion to apples and potato tubers.

2.3.3.1 Apples

We have used varieties of apples whose geometry approaches that of a sphere (Solomos 1987). Within the cultivar, we selected fruits whose equatorial and polar circumferences differed by <5%. In order to subject the data to experimental verification, we altered the rate of CO\textsubscript{2} output by decreasing the external O\textsubscript{2} concentration and comparing the values of CO\textsubscript{2} diffusivities. The experimental arrangements were those described by Burg and Burg (1965), with minor modifications (Solomos 1987, 1989). The geometrical configuration of the skin of the apple was assumed to be a hollow spherical shell. It is apparent from Eq. (2.10) that the concentration of CO\textsubscript{2} under the skin, along with the respiration rates and fruit dimensions, must be known, so that \(D'\) can be calculated. The concentration of CO\textsubscript{2} under the skin can be measured by inserting a hypodermic needle just under the surface of the fruit, while the concentration at the center is obtained by inserting a hypodermic needle through the calyx into the locules. In most of the apple cultivars we used, the gradient between the center and the subcutin was quite small (0.2–0.6%) (Solomos 1987). In the case of “Gala,” whose data are presented here, the gradient of CO\textsubscript{2} was between 0.1% and 0.2%, which falls within the experimental error for measuring CO\textsubscript{2}. It has been demonstrated that in the case of ethylene, the use of the concentration at the center to represent that under the skin introduced an insignificant error in the values of \(D'\) (Solomos 1989). Thus, the concentration of CO\textsubscript{2} under the skin is taken to be identical to that at the center. Table 2.8 shows the diffusion coefficient of CO\textsubscript{2} under different external O\textsubscript{2} concentrations. When the external O\textsubscript{2} concentration was decreased in steps from air to N\textsubscript{2}, this of course affected the rate of CO\textsubscript{2} output. It may be seen from Table 2.8 that the diffusivities of CO\textsubscript{2} under different O\textsubscript{2} levels are in reasonable agreement.

Apple fruit pose problems for evaluating the diffusivity of their intercellular spaces. Because of the small difference in CO\textsubscript{2} concentrations between the center
and subcutin, Eq. (2.8) cannot be used to calculate $D$. We thus proceeded to peel the fruit, blot it dry with filter paper, and then measure the rate of respiration and internal CO$_2$ concentration. Within about 6–8 h, the rate of CO$_2$ evolution was close to that of the intact fruit, probably because the dissolved CO$_2$ was dissipated. From the rate of CO$_2$ output and external and internal CO$_2$ concentrations, its diffusion coefficient in the intercellular spaces was calculated based on Eq. (2.8). The values obtained are presented in Table 2.9. Unfortunately the validity of these values cannot be tested experimentally because with time the outer layers of the fruit will form periderm, thus altering the internal concentration of CO$_2$.

### 2.3.3.2 Potato Tubers

We have used only “Russet Burbank” tubers because their geometry simulates a cylinder. (It should be stressed, however, that no tuber is exactly cylindrical.) The tubers were selected with the proviso that their length be greater than 11 cm and that the circumference, measured at several points along the tuber, not vary by more than 10% (Abdul-Baki and Solomos 1994). The CO$_2$ concentrations under the skin and at the center were measured by gluing two chromatographic septa, 11 mm in diameter, onto the surface in the middle of the tuber, each septum being 180° apart. Through the septa, two hypodermic needles were inserted, one at the center and the other under the skin. In addition the thickness of the lenticels was measured.
microscopically. From the rate of CO\textsubscript{2} output and the concentration of CO\textsubscript{2} under the skin, the diffusion coefficient of CO\textsubscript{2} in the skin was calculated using Eq. (2.11). Table 2.10 shows the values of the $D_{CO_2}$. It may be seen that there is appreciable variability between the tubers. These values are close to those reported previously for O\textsubscript{2} (Burton 1950). The validity of the data was tested by transferring the tubers from 10 to 27 °C. From the observed values of CO\textsubscript{2} concentration under the skin, and the values of $D_{CO_2}$ calculated from those obtained at 27 °C (Jost 1960), we calculated the rate of CO\textsubscript{2} output at 10 °C and compared it to that observed. The observed and calculated values of respiration are in good agreement (Table 2.11).

<table>
<thead>
<tr>
<th>Tuber no.</th>
<th>10 °C</th>
<th>27 °C</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>7.16</td>
<td>8.21</td>
</tr>
<tr>
<td>2</td>
<td>6.73</td>
<td>9.33</td>
</tr>
<tr>
<td>3</td>
<td>6.03</td>
<td>6.04</td>
</tr>
<tr>
<td>4</td>
<td>6.04</td>
<td>7.97</td>
</tr>
<tr>
<td>5</td>
<td>6.37</td>
<td>7.77</td>
</tr>
<tr>
<td>6</td>
<td>4.19</td>
<td>5.12</td>
</tr>
<tr>
<td>7</td>
<td>5.56</td>
<td>5.98</td>
</tr>
<tr>
<td>8</td>
<td>7.79</td>
<td>7.62</td>
</tr>
<tr>
<td>Avg</td>
<td>6.24</td>
<td>7.26</td>
</tr>
</tbody>
</table>

The values of $D_{CO_2}$ were calculated by inserting in Eq. (2.11) the observed fluxes and concentrations of CO\textsubscript{2} under the skin, along with dimensions of the tuber and skin thickness (0.012 cm)

<table>
<thead>
<tr>
<th>Tuber no.</th>
<th>27 °C</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>2.97</td>
</tr>
<tr>
<td>2</td>
<td>2.37</td>
</tr>
<tr>
<td>3</td>
<td>2.63</td>
</tr>
<tr>
<td>4</td>
<td>2.34</td>
</tr>
<tr>
<td>5</td>
<td>2.34</td>
</tr>
<tr>
<td>6</td>
<td>2.39</td>
</tr>
<tr>
<td>7</td>
<td>2.56</td>
</tr>
<tr>
<td>8</td>
<td>2.70</td>
</tr>
<tr>
<td>Avg</td>
<td>2.54</td>
</tr>
</tbody>
</table>

The theoretical fluxes were obtained by inserting in Eq. (2.11) the calculated values of $D_{CO_2}$ at 10 °C from those observed at 27 °C along with the theoretical CO\textsubscript{2} concentration under the skin, calculated as in Table 2.13, the dimensions of the tuber, and the concentration of CO\textsubscript{2} in the ambient atmosphere
The diffusion coefficient of CO$_2$ in the flesh was calculated from the values of CO$_2$ output, based on Eq. (2.9) (Table 2.12). The accuracy of these values was tested by calculating the concentration of CO$_2$ under the skin from Eq. (2.9) along with the observed concentrations of CO$_2$ at the center, and the calculated values of D$_{CO_2}$ at 10 °C from the data at 27 °C corrected for temperature (Jost 1960). Here too, the observed and calculated values are in reasonable agreement (Table 2.13).

### Table 2.12 Diffusion coefficient (cm$^2$·sec$^{-1}$×10$^{-4}$) of CO$_2$ in the flesh of potato tubers

<table>
<thead>
<tr>
<th>Tuber no.</th>
<th>10 °C</th>
<th>27 °C</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>1.67</td>
<td>1.90</td>
</tr>
<tr>
<td>2</td>
<td>2.17</td>
<td>2.23</td>
</tr>
<tr>
<td>3</td>
<td>2.63</td>
<td>3.10</td>
</tr>
<tr>
<td>4</td>
<td>2.68</td>
<td>2.90</td>
</tr>
<tr>
<td>5</td>
<td>2.90</td>
<td>2.46</td>
</tr>
<tr>
<td>6</td>
<td>2.30</td>
<td>2.67</td>
</tr>
<tr>
<td>7</td>
<td>3.65</td>
<td>3.81</td>
</tr>
<tr>
<td>8</td>
<td>1.96</td>
<td>2.10</td>
</tr>
<tr>
<td>Avg</td>
<td>2.50</td>
<td>2.65</td>
</tr>
</tbody>
</table>

### Table 2.13 Observed and calculated concentrations (μmoles·cm$^{-3}$) of CO$_2$ under the skin at 10 °C

<table>
<thead>
<tr>
<th>Tuber no.</th>
<th>Observed</th>
<th>Calculated</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>1.90</td>
<td>1.89</td>
</tr>
<tr>
<td>2</td>
<td>1.42</td>
<td>1.51</td>
</tr>
<tr>
<td>3</td>
<td>2.66</td>
<td>2.64</td>
</tr>
<tr>
<td>4</td>
<td>1.85</td>
<td>1.87</td>
</tr>
<tr>
<td>5</td>
<td>1.87</td>
<td>1.86</td>
</tr>
<tr>
<td>6</td>
<td>2.93</td>
<td>2.96</td>
</tr>
<tr>
<td>7</td>
<td>2.53</td>
<td>2.52</td>
</tr>
<tr>
<td>8</td>
<td>2.10</td>
<td>2.10</td>
</tr>
<tr>
<td>Avg</td>
<td>2.15</td>
<td>2.17</td>
</tr>
</tbody>
</table>

The theoretical values were obtained by inserting in Eq. (2.9) the calculated values of D$_{CO_2}$ from their value at 27 °C (Jost 1967), along with the observed CO$_2$ concentration at the center, and the specific respiration

The diffusion coefficient of CO$_2$ in the flesh was calculated from the values of CO$_2$ output, based on Eq. (2.9) (Table 2.12). The accuracy of these values was tested by calculating the concentration of CO$_2$ under the skin from Eq. (2.9) along with the observed concentrations of CO$_2$ at the center, and the calculated values of D$_{CO_2}$ at 10 °C from the data at 27 °C corrected for temperature (Jost 1960). Here too, the observed and calculated values are in reasonable agreement (Table 2.13).

### 2.4 Modeling for Appropriate Gas Environment in MAP

#### 2.4.1 General Considerations

MAP is an inexpensive way to generate controlled atmosphere (CA) conditions within the package. The CA environment is generated through the interactions between produce respiration, film permeability to gases, and the ratio between total film area and produce weight. MAP is a dynamic system in that the internal concentration of gases changes continuously until it reaches a steady state, i.e., where the
rates of O₂ and CO₂ fluxes equal their respective rates of utilization and production. Modeling thus includes a determination of the time it takes for the gases to reach their steady-state levels, which must equal their desired concentrations for the produce under consideration. However, the non-steady-state part of the modeling is of limited practical value and may be ignored. Modeling can be carried out under steady-state conditions.

At any time, the rate of changes in the concentrations of O₂ and CO₂ per unit volume of free gas space in the package can be expressed as:

\[
\begin{align*}
\frac{d[O_2]}{dt} &= \frac{P_{O_2} A \left([O_2]_{\text{out}} - [O_2]_{\text{in}}\right)}{V} - \frac{R_{O_2} W}{V} \quad (2.14) \\
\frac{d[CO_2]}{dt} &= -\frac{P_{CO_2} A \left([CO_2]_{\text{in}} - [CO_2]_{\text{out}}\right)}{V} + \frac{R_{O_2} W}{V} \quad (2.15)
\end{align*}
\]

where \([O_2]\) and \([CO_2]\), in ml/cm⁻³, are the concentrations of O₂ and CO₂, respectively; \(P_{O_2}\) and \(P_{CO_2}\), in ml/h cm² ml cm⁻³, are the permeabilities of the film to O₂ and CO₂; \(A\), in cm², is the area of the film; \(R_{O_2}\) and \(R_{CO_2}\), in ml kg⁻¹/h⁻¹, are the rates of O₂ uptake and CO₂ output, respectively; \(W\), in kg, is the weight of the produce; and \(V\), in cm³, is the free gaseous volume of the package (void volume).

Obviously when the system reaches steady state, the changes in CO₂ and O₂ concentrations in the package with time are zero; hence,

\[
\begin{align*}
R_{O_2} W &= P_{O_2} A \left([O_2]_{\text{out}} - [O_2]_{\text{in}}\right) \quad (2.16) \\
R_{CO_2} W &= P_{CO_2} A \left([CO_2]_{\text{in}} - [CO_2]_{\text{out}}\right) \quad (2.17)
\end{align*}
\]

### 2.4.2 Rate of Respiration

The solutions of Eqs. (2.14) and (2.15) require a precise knowledge of the rates of O₂ uptake and CO₂ evolution, which in turn vary with the concentrations of O₂ and CO₂, that is, \(R_{O_2} = f(O_2, CO_2)\) and \(R_{CO_2} = g(O_2, CO_2)\). Further, the effect of O₂ or CO₂ on the rate of respiration is also dependent on the stage of maturity. For instance, in preclimacteric “Gala” apples, the rate of CO₂ output decreases when the external O₂ concentration drops below 8.10 kPa (8%), whereas in the climacteric kind, the rate of CO₂ output is of zero order with respect to the external O₂ concentration up to 2.53 kPa (2.5%) (unpublished observations). The rates of O₂ uptake and CO₂ output can be determined using a flow-through system. Here, a stream of gas is passed through the tissue which is enclosed in a jar. The levels of O₂ and CO₂ in the outlet stream are monitored. This method is probably the most accurate. However, it is not practicable to measure the rate of respiration under a number of combinations
of O₂ and CO₂. Alternatively, the tissue may be enclosed in a vessel, and the changes in O₂ and CO₂ in the head space can be measured. At any instant, the change in the concentrations of O₂ and CO₂ will be dependent on the rate of respiration, the volume of the gas space in the vessel, and the weight of the tissue. Therefore,

\[ R_{O_2} = \frac{V_o}{W} \frac{d[O_2]}{dt} \]  

(2.18)

This method has the advantage that the rate of respiration can be determined under a variety of O₂ and CO₂ concentrations. However, if rapid changes in the rate of respiration are involved, they could introduce some uncertainty, especially with bulky plant organs, because of the large differences between the solubilities of O₂ and CO₂ in water. It is thus expected that the external O₂ levels will reach equilibrium between the concentrations in the intercellular gas spaces and the ambient atmosphere faster than will those of CO₂. It has been noted earlier that this can introduce appreciable experimental error in the values of RQ. Nevertheless, if appropriate ratios of the volume of the respiratory vessel to weight of tissue are chosen, it is possible that the concentration of gases in the ambient and fruit atmospheres will be close to equilibrium because the changes occur gradually. A number of authors have determined the rate of O₂ uptake by scrubbing the CO₂ in the vessel (Cameron et al. 1989; Henig and Gilbert 1975). Because of the absorption of CO₂, the pressure of the jar will decrease with time. This may introduce some experimental errors because of possible contamination from air during the withdrawal and subsequent injection of the gas into the gas chromatogram. Cameron (1989) measured the rate of O₂ depletion by enclosing an O₂ electrode in the jar, thus eliminating this source of experimental error.

Once the relationship between rates of O₂ uptake and CO₂ output as a function of both O₂ and CO₂ levels is determined, an expression is generated by various interpolation techniques. A number of interpolation methods have been used in the past to express the rates of O₂ uptake and CO₂ output as a function of O₂ and CO₂ concentrations. Henig and Gilbert (1975) divided the isotherms showing the percentage of gas versus time into linear and curvilinear segments. The latter part was plotted on semilog arithmetic paper, and both segments were subjected to regression analysis for the determination of the coefficients and intercepts. Hayakawa et al. (1975) expressed the rate of respiration in stepwise linear segments which were subsequently used to develop a predictive MAP model. Cameron (1989) fitted the O₂ depletion data to an exponential function, whereas Yang and Chinnan (1987, 1988a) used polynomial interpolations.

Unfortunately previously published modeling work was mainly concerned with intact tissue. There is a scarcity of experimental data regarding both the optimal MAP conditions and the effects of O₂ and CO₂ on the rate of respiration of tissue segments.

As mentioned above, slicing of tissues cut from such plant organs as tubers and roots invokes an immediate two- to fourfold increase in respiration over the parent organs (Laties 1978). In addition, there is a further two- to threefold increase with aging.
The latter increment depends on temperature and on whether the aging takes place with slices that are submerged in aerated liquid or in moist air (cf. Laties 1978). The facts that (1) slice respiration is mediated mainly by cytochrome oxidase with a $K_m$ for $O_2$ of 0.05 μM (Solomos 1988; Theologis and Laties 1978) and (2) the resistance to diffusion through the flesh is lower than that through the skin indicate that tissue slices at relatively low temperatures can be maintained at quite low $O_2$ concentrations. For instance, the diffusion of $O_2$ in potato flesh is about $2.9 \times 10^{-4}/cm^2 \sec^{-1}$ (Table 2.11). If it is assumed that at $10 \degree C$ the rate of $O_2$ uptake is $9 \mu l \ kg^{-1} \ h^{-1}$, and the ambient $O_2$ concentration is 2%, then the $O_2$ level at the center of a slice 2 cm thick will be about 0.4%, which will result in a $6.7 \mu M$ $O_2$ solution in the adjacent cells, a concentration that is unlikely to limit cytochrome oxidase. We have observed that the rate of $O_2$ uptake of sweet potato slices 2 mm thick at 25 °C is of zero order with respect to its external level until the latter decreases below 0.5% (Fig. 2.2).

The effect of temperature on MAP modeling must also be considered because it affects both the rate of respiration and film permeability to gases. The effects of temperature on plant respiration can be expressed as Arrhenius-type equations (James 1953). In chilling-sensitive tissues, there is an increase in the energy of activation at low temperatures (Lyons 1973). Further, in a number of tissues, low temperatures may induce a rise in respiration. A classic example is potato tubers, where storage at 1 °C evokes a rise in respiration above that observed at 10 °C (Isherwood 1973).

Changes in the permeability of gases through the film with temperature can also be expressed by an Arrhenius-type equation (Mannapperuma et al. 1991). The authors have determined the energy of activation of a number of commercially available films.

### 2.4.3 Steady-State Modeling

The most important aspect of MAP modeling is the design of suitable packaging for generating the requisite gas environment for long-term storage of the commodity. Usually, the establishment of the steady-state CA environment takes about 24 h, which is adequate for most commodities. In cases where the creation of the desired gas composition has to be accelerated, the package can be flushed with the appropriate gas mixture before sealing. It should be underlined that the time for the system to reach its final steady state is determined by the parameters that are used for the creation of the long-term desired gas composition. A detailed knowledge of the transient changes in the gas composition is of limited practical value, though very interesting from a theoretical point of view.

It has been noted above that under steady-state conditions, the concentrations of $O_2$ and $CO_2$ inside the package can be considered constant, although small changes occur gradually due to changes in the respiratory activity of the tissue under the new gas environment. Thus, $(d[O_2]_m/dt)$ and $(d[CO_2]_m/dt)$ are zero, and the equilibrium fluxes can be determined from Eqs. (2.16) and (2.17). It is apparent from these equations that the internal concentrations of $O_2$ and $CO_2$ will be determined from the rates
of O₂ uptake and CO₂ evolution, weight of the tissue, and area and permeability properties of the film. Combining Eqs. (2.16) and (2.17) we obtain:

\[
\frac{R_{O_2}}{R_{CO_2}} = \frac{P_{O_2}}{P_{CO_2}} \left[ \frac{[O_2]_{out}}{[CO_2]_{in}} - \frac{[O_2]_{in}}{[CO_2]_{out}} \right]
\] (2.19)

It is evident that both the RQ and the ratio of permeabilities of O₂ over CO₂ will be critical in establishing a particular CA environment. For most tissues, RQ is close to one, in particular for tissue slices of bulky plant organs such as tubers and roots (Laties 1978). Assuming a value for RQ of 1, Eq. (2.18) can be rearranged to become:

\[
[CO_2]_{in} = \frac{P_{O_2}}{P_{CO_2}} [O_2]_{out} + \frac{P_{O_2}}{P_{CO_2}} [O_2]_{in} - [CO_2]_{out}
\] (2.20)

A plot of \([O_2]_{in}\) against \([CO_2]_{in}\) will result in a straight line with a slope equal to the permeability ratio, as \([CO_2]_{out}\) can be neglected, and the \(\frac{P_{O_2}}{P_{CO_2}} [O_2]_{out}\) is constant. Figure 2.3 illustrates the relationship between \([O_2]_{in}\) and \([CO_2]_{out}\) for 1/2, 1/4, 1/5, and 1/6 permeability ratios of O₂ over CO₂. These ratios were chosen because they are the most common in commercially available films. For a successful MAP package, the combination of internal concentrations of O₂ and CO₂ will fall close to the line for a given permeability ratio.

Equations (2.16) and (2.17) show that the area of the film, along with the weight of the tissue, will be critical in establishing a desired MAP environment. If \(W/A\) is denoted by \(\rho\), then:

\[
[O_2]_{in} = \frac{R_{O_2}}{P_{O_2}} \rho (2.21)
\]

\[
[CO_2]_{in} = [CO_2]_{out} + \frac{R_{CO_2}}{P_{CO_2}} \rho (2.22)
\]

In this way, an appropriate \(W/A\) ratio can be selected to move the internal CO₂ and O₂ concentrations toward the point where the lines of Fig. 2.3 intersect the right-hand y-axis.

Jurin and Karel (1963) determined the steady-state internal oxygen concentration from the intercept of the plot of the experimental rates of respiration and flux across the film as a function of O₂ concentration. Cameron (1989) and Cameron et al. (1989) fitted the curve showing oxygen depletion versus time to an exponential equation:

\[
[O_2] = a \left[ 1 - e^{-\left(\frac{bt}{c}\right)^d} \right]
\] (2.23)

where \(a\), \(b\), and \(c\) are constants. The rate of respiration at steady state was calculated by multiplying the time derivative of Eq. (2.23) by the \(V/W\) ratio, where \(V\), in lit, and
$W$, in kg, are the void volume of the vessel and weight of tomato fruits, respectively. The transient changes were ignored; only steady-state modeling was considered. It should be noted that Eq. (2.23) may not always be appropriate to use with plastic bags because of the changes in the void volume due to film shrinkage. Changes in $V$ are produced by the decrease in the internal pressure due to differences in the permeabilities of $O_2$ and $CO_2$. This necessitates a decrease in volume so that the internal total gas pressure equals the ambient pressure (see later). Equations (2.16) and (2.17) are more appropriate because the volume is not a variable.

In summary, for modeling an appropriate MAP package, first the desired concentration of gases for a particular commodity can be selected from the compilation of previous data (Isenberg 1979; Kader 1985; Saltveit 1989). Then from the values of respiration under the chosen MAP environment, the appropriate film and $W/A(\rho)$ ratio can be determined.

2.4.4 Dynamic Modeling

Non-steady-state modeling can predict both the time from the start until the virtual steady-state is established, and the steady-state concentrations of $O_2$ and $CO_2$ in the package. In order to generate the appropriate expressions, the equations expressing the rate of respiration as $f(O_2, CO_2)$ must be inserted into Eqs. (2.14) and (2.15). The results in the literature differ somewhat (Chinnan 1989; Hayakawa et al. 1975; Mannapperuma et al. 1991). These differences could be partly biological in nature.

Fig. 2.3 Steady-state relationship between the internal concentrations of $CO_2$ and $O_2$
because of the inherent variability in biological material, and because of the limited number of determinations that are usually used. The differences could also be due to physical considerations in assessing the rate of respiration and changes in gas concentrations inside the package during the transient stage.

In order to illustrate the latter point, we assume a solid sphere with a diffusion coefficient similar to that for $O_2$ in the “Russet Burbank” potato tuber ($2.94 \times 10^{-4} \text{ cm}^2 \text{ sec}^{-1}$). Further, at zero time, the sphere contains no $O_2$ and is transferred to a vessel where the $O_2$ concentration is maintained constant at $9.1 \mu$moles cm$^{-3} O_2$ (air concentration at $10 \, ^\circ C$). It is also assumed that oxygen is not utilized by the tissue. It can be shown that for boundary conditions $C(R,t) = C_0, t > 0$, and $C(0,t) = 0$ for $0 < t < t_2$, and initial conditions $C(r,0) = 0$, the solution of Eq. (2.2) is:

$$C(r,t) = C_0 + \frac{2RC_0}{\pi r} \sum_{n=1}^{\infty} \frac{(-1)^n}{n} \sin \frac{n\pi r}{R} \cdot \exp \left( -\frac{n^2 \pi^2}{R^2} \cdot Dt \right)$$ (2.24)

where $C_0$, in $\mu$moles·cm$^{-3}$, is the concentration of $O_2$ in the ambient atmosphere; $R$, in cm, is the radius of the sphere; $t$, in sec, is the time; and $D$, in cm$^2$ sec$^{-1}$, is the diffusion coefficient. It may be seen from Fig. 2.4a and b that even after 10 min, the concentration of $O_2$ at $r = 1$ is almost zero. Figure 2.4b demonstrates the distribution of $O_2$ along the radius after 1 h. It should be noted that the gradient would have been steeper if the utilization of $O_2$ had been incorporated into the solution of Eq. (2.2) and if the resistance to $O_2$ diffusion of the skin had also been included. Even if the initial $O_2$ distribution is not zero, the concentration gradient could be appreciable (Crank 1970).

It is likely that under rapid changes in the external $O_2$ concentration in a closed system, an appreciable concentration gradient of oxygen along the organ will develop. Under these conditions, the rate of respiration of the cells on the periphery will differ from those at the center of the organ because of the substantial differences in $O_2$ concentration. Further, the changes in respiration calculated from the gas isotherms may represent part of the respiration of the organ, because the distribution of the cells at the center may not be perceived.

It has been noted above that because of the differences in $O_2$ and $CO_2$ permeabilities through the film, a partial vacuum is generated inside the package which in turn produces a decrease in void volume in order that the internal pressure may equal the ambient pressure. In short, the void volume is also a function of time, and Eq. (2.14) should be written as follows:

$$\frac{d[O_2]}{dt} = P_{O_2}A \left( [O_2]_{\text{out}} - [O_2]_{\text{in}} \right) - \frac{R_{O_2}W}{V(t)}$$ (2.25)

A note of caution is also appropriate regarding the global validity of the rates of respiration calculated from the gas isotherms. In general, a number of interpolations produce a unique function. This, however, may not be the case for all methods of interpolation (Lancaster and Salkauskas 1986). Although the uniqueness of the local expression may be assured, this may not necessarily reflect the biochemical
behavior of the system. For instance, the rate of respiration of a number of plant tissues is of zero order at concentrations of $O_2$ from 15% to 100% (Burton 1974; James 1953; Tucker and Laties 1985). If the local expressions reflected the biochemical events that underly plant respiration, the extension of the interpolation
to concentrations of $O_2$ larger than those in air will result in respiration being independent of $O_2$.

It should also be noted that the relationship between $O_2$ and respiration is enzymatic in nature and may involve more than one terminal oxidase whose affinities for oxygen may differ. Furthermore, the suppression of respiration may be the result of a metabolic depression involving alterations in the kinetic properties and/or amount of key regulatory respiratory enzymes (Storey and Storey 1990). It may thus be more appropriate to develop mathematical expressions reflecting the kinetics of multienzyme sequences (Goldbeter 1991) rather than the usual interpolating techniques that are frequently used in the literature.

2.4.4.1 Experimental Dynamic MAP Modeling

The literature on dynamic MAP modeling has been reviewed previously (Chinnan 1989; Mannapperuma et al. 1991). Here a limited amount of previous research, representing different approaches to deriving predictive mathematical expressions, will be considered.

Deily and Rizvi (1982) produced analytical formulae for predicting the gas concentration and the time necessary to reach the final dynamic equilibrium for peach fruits. They observed that the $O_2$ depletion isotherm consists of linear and exponential segments with an inflection point at about 5% $O_2$ and 20% $CO_2$. Further, the rate of respiration was unaffected by $CO_2$ concentrations in the range of 1–27%. Since the optimal MAP environment for peach storage was found to be 10–15% $O_2$ and 15–25% $CO_2$, and since the rate of respiration is constant under these conditions, the authors solved Eqs. (2.14) and (2.15) for constant \( R_{O_2} \) and \( R_{CO_2} \). The analytical formulae derived for calculating $O_2$ and $CO_2$ are:

\[
y(t) = \overline{y} + (y_a - \overline{y}) \cdot \exp\left(-AP_{O_2} t / V\right)
\]

\[
z(t) = \overline{z} + (z_a - \overline{z}) \cdot \exp\left(-AP_{CO_2} t / v\right)
\]

where \( \overline{y} \) and \( \overline{z} \) are the steady-state levels of $O_2$ and $CO_2$, calculated from the steady-state solution of Eqs. (2.14) and (2.15) and from limit \( (y(t)/t \to \infty) \). \( y_a \) and \( z_a \) are the internal concentrations of $O_2$ and $CO_2$ at \( t = 0 \). The analytical formulae were tested by comparing the experimental and predicted gas concentrations using different films. Table 2.14 shows a good agreement between observed and calculated values.

Henig and Gilbert (1975) solved Eqs. (2.14) and (2.15) numerically using the experimental results of the respiration rate as a function of external $O_2$ and $CO_2$ concentrations. The authors validated the computer modeling with the experimental data. The experimental results with a FV-71 film package were in good agreement with the computer-predicted results (Fig. 2.5) (Henig and Gilbert 1975). The authors also tested the validity of the computer model by altering the variables of the inputs, for example, permeability, weight/void volume ratio, and film area. Their results
Table 2.14 Parameters and results of analytical and experimental determination of model packages of peach fruits

<table>
<thead>
<tr>
<th>Parameters</th>
<th>Package types</th>
<th>Film overlaps on foam trays</th>
</tr>
</thead>
<tbody>
<tr>
<td></td>
<td>Bags</td>
<td>Super-L-bags</td>
</tr>
<tr>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>$W$</td>
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<td>212.30</td>
</tr>
<tr>
<td>$R_y$</td>
<td>7.84</td>
<td>7.84</td>
</tr>
<tr>
<td>$R_z$</td>
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<td>7.55</td>
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<tr>
<td>$S$</td>
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<td>0.11</td>
</tr>
<tr>
<td>$V$</td>
<td>2.34</td>
<td>2.32</td>
</tr>
<tr>
<td>$K_y$</td>
<td>166.67</td>
<td>166.67</td>
</tr>
<tr>
<td>$K_z$</td>
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<td>200.00</td>
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</tr>
<tr>
<td>$CO_2%$</td>
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<td>7.05</td>
</tr>
<tr>
<td>$t$</td>
<td>96.00</td>
<td>108.00</td>
</tr>
</tbody>
</table>

$W$, $S$, and $V$ are the weight, surface, and void volume of the package, respectively. $R_y$ and $R_z$ are the rates of $O_2$ uptake and $CO_2$ output, respectively, and $K_y$ and $K_z$ are the permeabilities to $O_2$ and $CO_2$, respectively, of the films. $\hat{y}$ and $\hat{z}$ are the steady-state levels of $O_2$ and $CO_2$, respectively. $t = \text{time after packaging (h)}$

From Deily and Rizvi (1982)

---

Fig. 2.5 Changes with time in $O_2$ and $CO_2$ concentrations in a RMF-61 film package of tomato fruits (From Henig and Gilbert 1975)
showed that the predicted steady-state values of CO\textsubscript{2} and O\textsubscript{2} concentrations were similar to those expected.

Hayakawa et al. (1975) derived an analytical solution of Eqs. (2.14) and (2.15) using Laplace transforms. The rate of respiration was expressed as linear segments:

\[
R_{\text{O}_2} = a_i \left[ O_2 \right] + p_i \left[ CO_2 \right] + q_i 
\]

\[
R_{\text{CO}_2} = d_i \left[ O_2 \right] + e_i \left[ CO_2 \right] + f_i 
\]

where \( a_i, p_i, q_i, d_i, e_i, \) and \( f_i \) are constants, and \([O_2]\) and \([CO_2]\) are the analytical expressions determining the O\textsubscript{2} and CO\textsubscript{2} levels. Because of computational complications, the authors assumed that the rate of O\textsubscript{2} uptake of tomato fruits was not critically affected by CO\textsubscript{2}; hence, \( p_i = 0 \). Similarly it was assumed that the rate of CO\textsubscript{2} output was not significantly affected by the external O\textsubscript{2} levels. There is some uncertainty concerning the latter assumption because usually the rate of CO\textsubscript{2} evolution parallels that of O\textsubscript{2} uptake as a function of external O\textsubscript{2} concentrations up to the inflection point. Nevertheless, the predicted transient changes in O\textsubscript{2} and CO\textsubscript{2} concentrations were similar to those observed experimentally (Fig. 2.6).

Yang and Chinnan (1987) measured the rates of O\textsubscript{2} uptake and CO\textsubscript{2} output under 20 combinations of external O\textsubscript{2} and CO\textsubscript{2} concentrations. These data were subsequently used to develop a computer-predictive model by expressing the rates of O\textsubscript{2} uptake and CO\textsubscript{2} output as a second-degree polynomial of O\textsubscript{2}, CO\textsubscript{2}, and time (Yang and Chinnan 1988a):

![Fig. 2.6 A comparison between experimental and computed O\textsubscript{2} and CO\textsubscript{2} concentrations in a RMF-61 film package of tomato fruits (From Hayakawa et al. 1975)](image_url)
$R_{O_2} = a_0 + a_1C_o + a_2C_c + a_3t + a_4C_o^2 + a_5C_c^2 + a_6t^2 + a_7C_oC_c + a_8C_c^2 + a_9C_c \, t \tag{2.30}$

where $C_o$ and $C_c$ are the concentrations of O$_2$ and CO$_2$, respectively, and $a_0, a_9$ are constants. The calculated values were tested by comparing them with the experimental observations at two arbitrary combinations of O$_2$ and CO$_2$ levels (Fig. 2.7). The prediction of the steady-state concentrations of O$_2$ and CO$_2$ was achieved by iterative techniques which minimize the sum of the squares of the O$_2$ and CO$_2$ fluxes at short time intervals as the system approaches steady state (Yang and Chinnan 1988b). An innovative aspect of this work is the development of expressions to predict quality attributes, such as color, as a function of O$_2$ and CO$_2$. This is very useful for determining the apparent $K_m$ for O$_2$ of the enzyme(s) whose activity is restricted by O$_2$, thus producing a slowing of metabolic reactions in plant senescence in general and fruit ripening in particular.

### 2.5 Effects of Hypoxia on Plant Tissues

Hypoxia affects a large number of metabolic activities in plant tissues, for example, the induction and suppression of gene expression (Bailey-Serres and Chang 2005; Geigenberger 2003; Giovannoni 2004; Klok et al. 2002; Liu et al. 2005; van Dongen...
et al. 2009). Genes induced by hypoxia include anoxic proteins such as ADH (Kanellis et al. 1990). Conversely, hypoxia also suppresses the synthesis of existing proteins, such as those involved in cell wall synthesis, e.g., cellulase and polygalacturonase. In climacteric fruit ripening in general, its most profound effect lies in its suppression of the induction of the C2H4 onset. In apples, for example, the delay of the climacteric onset is initiated when the oxygen concentration falls below 8% (Fig. 2.8). Obviously, the effects of hypoxia are saturable with respect to oxygen.

2.6 Concluding Remarks

Substantial progress has been made in our understanding of the molecular aspects underlying the beneficial effects of low O₂ and/or high CO₂ on the shelf life of plant tissues. These include the induction of a number of genes as well as the suppression of the genes involved in the synthesis of existing proteins. At present, however, work still remains to be done regarding the nature of genes that are suppressed by hypoxia. This work will in turn shed light on the molecular aspects of the beneficial effects of MAP on plant tissues.

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